



**POLITECNICO**  
MILANO 1863

## Dynamics and Control of Chemical Processes

Prof. Davide Manca  
Chemistry, Material and Chemical Engineering Department, "G. Natta"  
Politecnico di Milano

### Lab #1

#### Exercise 1

A biological process is operated in a batch reactor characterized by the growth of biomass (B) at a loss of substrate (S). The material balances for the two species are:

$$\begin{cases} \frac{dB}{dt} = \frac{k_1 BS}{k_2 + S} \\ \frac{dS}{dt} = -k_3 \frac{k_1 BS}{k_2 + S} \end{cases}$$

Determine the dynamics of both the substrate and biomass over 15 h, knowing that:

$$k_1 = 0.5 \text{ h}^{-1}$$

$$k_2 = 10^{-7} \text{ kmol/m}^3$$

$$k_3 = 0.6$$

The initial conditions are:

$$\begin{cases} B(0) = 0.03 \text{ kmol/m}^3 \\ S(0) = 4.5 \text{ kmol/m}^3 \end{cases}$$

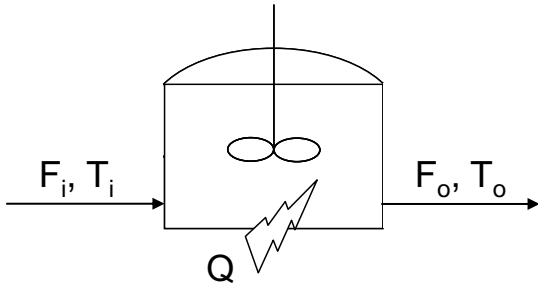
Solve the problem in Matlab. Modify the parameters for the error control of the ordinary differential system by adopting a relative tolerance of  $10^{-8}$  and an absolute one of  $10^{-12}$  (respect to the default Matlab values). Compare the two dynamics.

#### Exercise 2

Consider an intermediate storage tank that is perfectly mixed (CST) and heated.

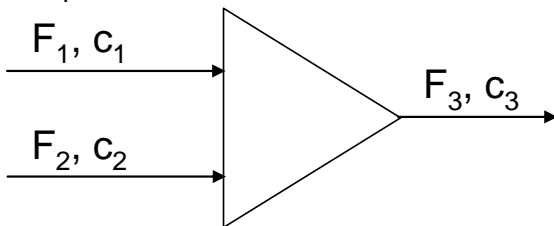
Evaluate the dynamics of the outlet temperature after a step disturbance of 30 °C on the inlet temperature, given the following data:

- Heat power supplied to the system:  $Q = 1 \text{ MW}$
- Inlet flowrate:  $F_i = 8 \text{ kmol/s}$
- Mass holdup of the CST:  $m = 100 \text{ kmol}$
- Specific heat of the mixture:  $cp = 2.5 \text{ kJ/kmol K}$
- Inlet temperature:  $T_i = 300 \text{ K}$



### Exercise 3

Let us consider the mixing of two streams featuring different concentrations of the same component.



Input data:

- Stream 1:  $F_1 = 2 \text{ m}^3/\text{h}$ ;  $c_1 = 0.5 \text{ kmol}/\text{m}^3$
- Stream 2:  $F_2 = 10 \text{ m}^3/\text{h}$ ;  $c_2 = 6 \text{ kmol}/\text{m}^3$
- Volume of the mixer:  $V_{\text{mixer}} = 12 \text{ m}^3$

Determine the outlet concentration dynamics from the mixer when the flowrate,  $F_1$ , varies linearly with the time as follows:  $F_1 = 0.04 \times t$ , up to the maximum value of:  $20 \text{ m}^3/\text{h}$ .

### Exercise 4

A side reaction occurs in a storage tank. The variations of conversion ( $z$ ) and temperature ( $\theta$ ) can be described by the following formula:

$$\begin{cases} \frac{dz}{d\tau} = \frac{\psi}{B} (1-z)^n h(\theta) \\ \frac{d\theta}{d\tau} = \psi (1-z)^n h(\theta) - \theta \end{cases}$$

In these reactions,  $B$  is the heat of reaction;  $n$  is the reaction order;  $\psi$  the ratio between the reaction heat and the heat removed by heat exchange;  $\varepsilon$  is the reaction activation energy;  $h$  is the exponential term of the reaction kinetics:

$$h(\theta) = \exp\left[\frac{\theta}{1 + \varepsilon\theta}\right]$$

All the variables are non-dimensional.

Evaluate the temperature dynamics when  $\psi$  varies between 0.35 and 0.65, with the following parameter values:

- $n = 1$
- $B = 20$
- $\varepsilon = 0.05$

The initial conditions are:

- $z(0) = 0$
- $\theta(0) = 1$ .