Prof. Davide Manca – Politecnico di Milano

#### **Dynamics and Control of Chemical Processes**

### Solution to Lab #1

# Introduction to System Dynamics



### E1 – Dynamics of a biological system

A biological process is run in a batch reactor where the biomass (B) grows by feeding on the substrate (S). The material balances for the two species are:

$$\begin{cases} \frac{dB}{dt} = \frac{k_1 BS}{k_2 + S} \\ \frac{dS}{dt} = -k_3 \frac{k_1 BS}{k_2 + S} \end{cases}$$

With:  $k_1 = 0.5 \text{ h}^{-1}$   $k_2 = 10^{-7} \text{ kmol/m}^3$   $k_3 = 0.6$ 

The initial conditions are:

 $\begin{cases} B(0) = 0.03 \text{ kmol/m}^3\\ S(0) = 4.5 \text{ kmol/m}^3 \end{cases}$ 



### E1 - Aim

• Determine the dynamic evolution of both biomass and substrate over a time interval of 15 h.

Use Matlab to solve the ordinary differential equations (ODE) system: (i) with the standard precision (*i.e.* by default) for both absolute and relative tolerances. (ii) Modify those tolerances with a relative tolerance of 1.e-8 and an absolute one of 1.e-12. Compare the two dynamics and provide a comment about them.



### **Integration of ODE in MATLAB**

To integrate the ordinary differential system one can use the functions implemented in MATLAB:

ode15s: for the integration of stiff systems

[t,y] = ode15s(@(t,y)myFun(t,y,params),tSpan,y0,options)

**ode45**: for the integration of non-stiff systems.

[t,y] = ode45(@(t,y)myFun(t,y,params),tSpan,y0,options)



## **Integration of ODE in MATLAB**

- Where:
  - t = time
  - y = the dependent variables matrix (each column represents a variable)
  - myFun = name of the ODE function
  - tSpan = integration time span [tMin tMax]
  - y0 = vector of initial conditions, *e.g.*, [B0 S0]
  - params = list of optional parameters for the solution of the differential system (e.g., k<sub>1</sub>, k<sub>2</sub>, k<sub>3</sub>) [params vector must however be always present even if no specific parameters are used)
  - options = options for the integrator

```
options = odeset('RelTol', 1E-8, 'AbsTol', 1E-12)
```



### **MATLAB code**

#### Main k1 = 0.5;% [h−1] $k^2 = 1E - 7;$ % [kmol] k3 = 0.6;8 [-] tSpan = [0 15]; % [h] y0 = [0.03 4.5]; % [kmol] y0(1) = B; y0(2) = S options = odeset('RelTol', 1E-8, 'AbsTol', 1E-12); [t,y] = ode45(@(t,y)Sisdif(t,y,k1,k2,k3),tSpan,y0,options);B = y(:, 1);S = v(:, 2);



### **MATLAB code**

#### <u>Sisdif</u>

```
function dy = Sisdif(t,y,k1,k2,k3)
dy = zeros(2,1); % column vector
B = y(1);
S = y(2);
dy(1) = k1*B*S / (S + k2);
dy(2) = - k3 * dy(1);
```



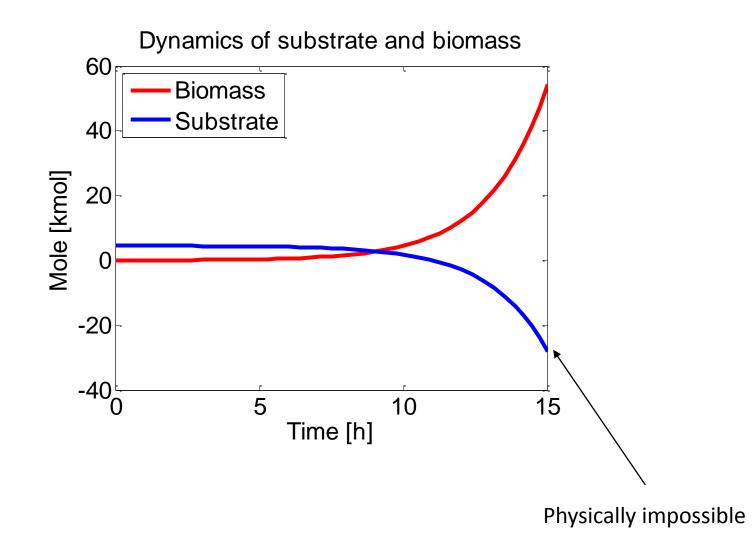
### **MATLAB code**

#### **Results display**

```
figure(1)
plot(t,B,'r',t,S,'b','LineWidth',3)
set(gca, 'FontSize', 18)
legend('Biomass', 'Substrate', 2)
xlabel('Time [h]')
ylabel('Mass [kmol]')
title('Dynamics of substrate and biomass')
grid off
saveas(figure(1), 'Biological System.emf')
                                        Advice: do not use the
                                            extension .fig
```

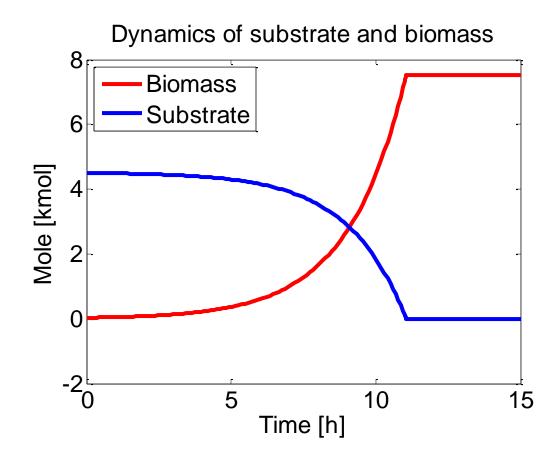


### **Dynamics of a biological system (1)**





### **Dynamics of a biological system (2)**





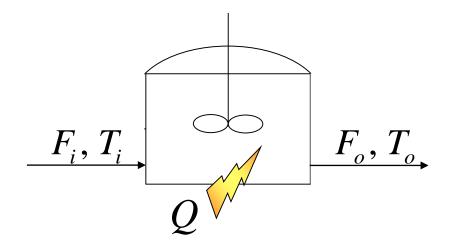
## E2 – Dynamics of a perfectly mixed tank

An intermediate tank is perfectly mixed (*i.e.* it is a continuously stirred tank, *aka* CST) and heated. Determine the dynamics of the outlet temperature when there is a step disturbance of 30 °C in the inlet temperature, with:

- Heating power: Q = 1 MW
- Inlet flowrate:  $F_i = 8 \text{ kmol/s}$
- CST mass holdup: m = 100 kmol
- Specific molar heat: cp = 2.5 kJ/kmol K
- Initial inlet temperature:  $T_i = 300 \text{ K}$



### **Modelling of the system**



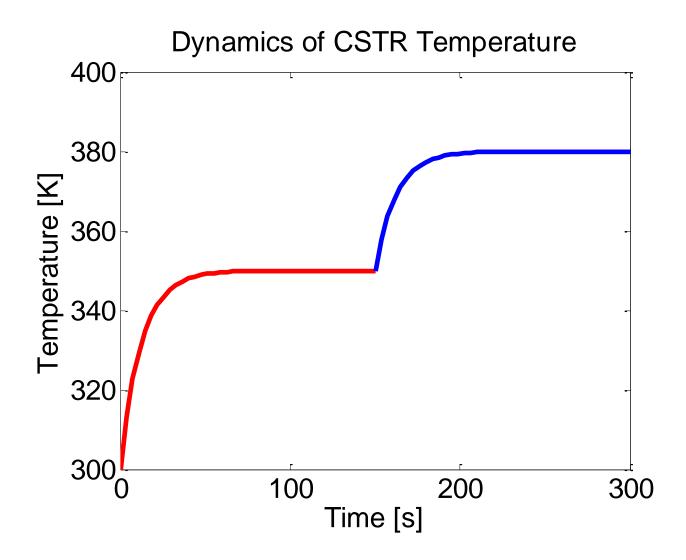
Mass balance:

Energy balance:

$$F_{i} = F_{o}$$
$$m c_{p} \frac{dT}{dt} = -F_{o} c_{p} \left(T_{o} - T_{i}\right) + Q$$

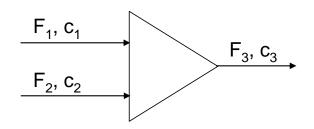


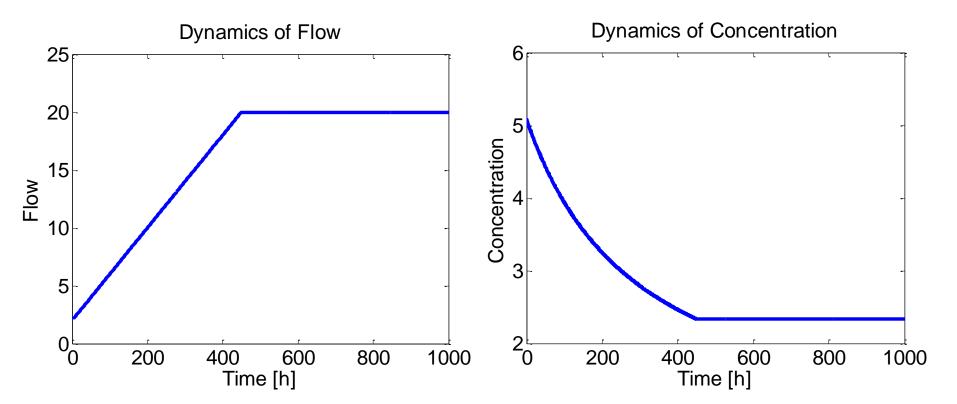
### **Results**













© Davide Manca – Dynamics and Control of Chemical Processes – Master Degree in ChemEng – Politecnico di Milano

### **E4** –**Runaway dynamics**

